

USING MRI TO STUDY *IN SITU* OIL RECOVERY DURING CO₂ INJECTION IN CARBONATES

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ABSTRACT

Fluid flow behavior during enhanced oil recovery experiments in chalk utilizing waterflooding and subsequent injection of CO₂ at miscible conditions was investigated in a n-Decane/deuterium oxide brine system at different wettabilities. During low rate waterflood, fluid saturation distributions were monitored *in situ* as function of time using high spatial resolution Magnetic Resonance Imaging (MRI). At S_{or, D2O}, CO₂ at either liquid or supercritical conditions was subsequently injected at low flow rate. 3D *in situ* images of the displacement processes indicated that the residual oil after waterflooding was contacted by and mixed with the CO₂ during continued flooding. This caused swelling of the oil phase, oil bank formation and improved sweep efficiency. The EOR potential for the chalk used in these experiments ranged from 17.1 % OOIP to 67.1 % OOIP depending on the wettability and the initial core saturations. Material balance measurements were used to calculate fluid saturations, and the results exhibited improved sweep efficiency and increased oil recovery.

INTRODUCTION

Injection of CO₂ in mature oil fields has proven to be an efficient EOR method due to its miscibility properties at high pressures and its ability to increase the mobility of the oil phase. In fractured carbonate reservoirs, parameters such as matrix permeability, wettability, reservoir pressure and temperature, initial water saturation, fracture-matrix geometry, production rates and oil and solvent viscosities and densities have great impact on oil recovery and sweep efficiency (Li (2000), Slobod (1964), Thompson (1969), Firoozabadi (1994), Jamshidnezhad (2004), Holm (1986), Asghari (2008)). Due to the complexity of the recovery mechanisms involved during CO₂ injection, the need for *in situ* data is of great importance in order to fully understand the displacement process.

In this study, waterfloods and subsequent CO₂ injections in low-permeable chalk at different wettabilities have been conducted at either liquid or supercritical conditions and above the reported Minimal Miscibility Pressure (MMP) for the system to ensure miscibility with the oil phase. High spatial resolution Magnetic Resonance Imaging (MRI)

has been utilized to calculate fluid saturations and to qualitatively monitor the displacement processes. The main objective of the study was to investigate the displacement process *in situ* and to determine the enhanced oil recovery potential from the CO₂ injection. A part of the study was to compare the effects from using supercritical CO₂ and liquid CO₂ and to study the *in situ* effects from injecting CO₂ at S_{wi} and $S_{or, D20}$.

EXPERIMENTAL

Four 3.81 cm diameter Portland Chalk core samples were oven dried for two days at 90°C, evacuated and saturated with synthetic brine. Porosity was calculated from weight measurements and absolute permeability to brine was measured using a Hassler type core holder. Three of the cores were drained to S_{wi} and aged using low rate injection of North Sea light crude oil at 80°C for selected periods of time to reach less water-wet and neutral-wet conditions. A more detailed description of the Portland chalk is found in Ekdale (1993), and the ageing process is described in Graue (1999), Graue (2002) and Aspenes (2003). One core was left at strongly water-wet conditions. Basic core properties, including length, diameter, porosity, absolute permeability to brine and Amott Indices after ageing are listed in Table 1.

Table 1. Core Properties.

Core Name	Length [cm]	Diameter [cm]	Porosity [%]	Permeability [mD]	Amott Index [frac.]
P1	10.02	3.81	48.4	3.96	0.29
P2	10.02	3.80	47.9	4.61	0.25
P7	10.00	3.81	48.4	3.56	1.00
G23	6.01	3.80	47.6	4.30	0.15

The four core samples were prepared for the MRI experiments by substituting brine with deuterium oxide brine in order to distinguish the water phase from the oil phase in the MRI, and thus the measured MRI intensities during waterfloods could be related to oil saturation. The cores were finally drained with n-Decane to reach S_{wi} . Fluid properties, including brine compositions and densities and viscosities at relevant temperatures and pressures are listed in Table 2.

The critical point of CO₂ is at 31.1 °C and 7398 kPa. Minimum Miscible Pressure (MMP) for the n-Decane/CO₂ system has been determined at 35 °C and 7329 kPa by Asghari (2008) and at 37.8 °C and 7894 kPa by Ayirala (2005). To ensure liquid properties of CO₂, the temperature and pressure were selected at 23 °C and 8274 kPa, respectively. To ensure supercritical properties, temperature and pressure were selected to 40 °C and 8274 kPa, respectively. All injection rates were set to 2 ml/h, corresponding to a frontal velocity of approximately 0.2 ft/d, to minimize fingering effects (Rathmell (1971)).

Table 2. Fluid Properties.

Fluid	Brine	D ₂ O Brine	Crude oil	n-Decane	CO ₂
Composition	5.0 wt% NaCl 3.8 wt% CaCl ₂ 0.1 wt% NaN ₃	5.0 wt% NaCl 3.8 wt% CaCl ₂	-	-	-
Density [g/cm ³] at 20°C	1.05	1.18	0.85	0.73	0.002
Density [g/cm ³] at 8274 kPa, 40°C	-	-	-	0.72	0.314
Viscosity [cP] at 20°C	1.09	1.10	14.3	0.92	0.015
Viscosity [cP] at 8274 kPa, 40°C	-	-	-	0.76	0.024
Viscosity [cP] at 80°C	-	-	2.7	-	-

During low rate, high pressure waterflood and subsequent injection of either liquid or supercritical CO₂ in three of the core samples, Magnetic Resonance Imaging (MRI) was used

- 1) to image fluid saturation distributions *in situ*, and
- 2) to investigate oil recovery mechanisms *in situ*.

In one core sample, supercritical CO₂ was injected at S_{wi} . Table 3 summarizes the Amott indices and the initial oil saturations of the core samples and the injection properties of the CO₂.

Table 3. Injection Data.

Core Name	Amott Index	$S_{o, wi}$ [%]	Temperature [°C]	CO ₂ State	CO ₂ Injection
P1	0.29	80.1	40	Supercritical	S_{wi}
P2	0.25	75.0	40	Supercritical	$S_{or, D2O}$
P7	1.00	69.8	23	Liquid	$S_{or, D2O}$
G23	0.15	79.9	23	Liquid	$S_{or, D2O}$

Figure 1 shows a schematic of the experimental setup. The core holder was installed horizontally in the MRI and connected to the two injection pumps and a third pump controlling the confining pressure. The pumps were operated by a laptop computer, and output pressures, injection rates, injected volumes and temperature were logged continuously. The outlet end of the core holder was connected to a fraction collector through a back pressure regulator, allowing the system to be pressurized.

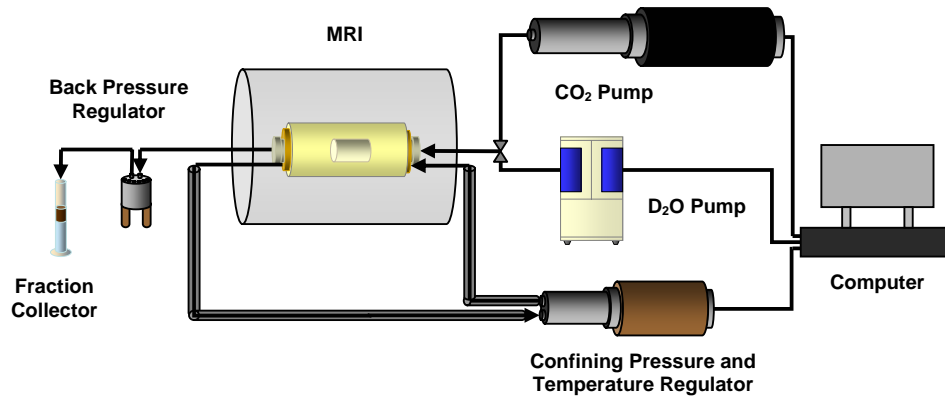


Figure 1: A schematic of the experimental setup.

RESULTS AND DISCUSSION

Table 4 lists initial and endpoint oil saturations and recovery factors from the waterfloods and CO₂ injections. From the table, injection of supercritical CO₂ at S_{wi} (in core plug P1) yields the lowest total recovery (67.1 % OOIP) of the four core samples. The most efficient oil recovery, 93.6 % OOIP, was obtained by waterflooding followed by CO₂ injection at supercritical conditions in the less water-wet core plug P2.

Table 4. Production Data.

Core Name	P1	P2	P7	G23
Amott Index	0.29	0.25	1.00	0.15
$S_{o, wi}$ [% PV]	80.1	75.0	69.8	79.9
$S_{or, D2O}$ [% PV]	-	26.9	25.2	53.2
$S_{w, or, D2O}$ [% PV]	-	73.1	74.8	46.8
$R_{f, D2O}$ [% OOIP]	-	64.1	63.9	33.4
$S_{or, CO2}$ [% PV]	26.4	4.8	13.3	20.3
$S_{w, or, CO2}$ [% PV]	24.6	59.0	47.0	22.7
$R_{f, CO2}$ [% OOIP]	67.1	29.5	17.1	41.2
$R_{f, total}$ [% OOIP]	67.1	93.6	81.0	74.6

Injection of supercritical CO₂ at $S_{or, D2O}$ at less water-wet conditions (core plug P2) provides the lowest $S_{or, CO2}$ (4.8 % PV) and proves to be the most efficient production strategy compared to injection of liquid CO₂ at $S_{or, D2O}$ at strongly water-wet conditions (core plug P7 with $S_{or, CO2}$ at 13.3 % PV) and to injection of liquid CO₂ at $S_{or, D2O}$ at near neutral-wet conditions (core plug G23 with $S_{or, CO2}$ at 20.3 % PV). Total oil recovery from injection of liquid CO₂ at $S_{or, D2O}$ is 81.0 % OOIP at strongly water-wet conditions (core plug P7) and 74.6 % OOIP at near neutral-wet conditions (core plug G23).

Figure 2 shows 2D and 3D MRI images of the oil saturation dynamics during injection of supercritical CO₂ at S_{wi} as function of injected pore volumes in the less water-wet core plug P1. The bright areas (yellow and red) indicate high oil saturation, and the dark areas (blue) indicate low oil saturation. The effluent production from D₂O injection (red line) and from CO₂ injection (black line) at each time step is indicated by the average oil saturation development in the core in the lower left corner of each time step. The injection of CO₂ causes swelling of the oil phase, seen as bright green and red areas near the inlet end in image 2, 3 and 4. The CO₂ enters the core in a piston-like displacement, leaving the residual oil and water saturations behind the CO₂ front.

Figure 3 and Figure 4 show 2D and 3D MRI images of the oil saturation dynamics during waterflood (red) and the following injection of supercritical CO₂ (black) in the less water-wet core P2, respectively. The waterflood images in Figure 3 show that the water enters the core in a piston-like displacement, leaving residual oil saturation of 26.9 % PV. MRI intensity as function of oil saturation during a waterflood in a water-oil system does not show the same non-linear response as for the water-oil-CO₂ system. Thus, the MRI signal does not disappear as in Figure 2. From Figure 4 oil swelling is observed as a bright green area moving through the core as the CO₂ enters the core, leaving a residual oil saturation of 4.8 % PV.

Figure 5 and Figure 6 show 2D and 3D MRI images of the oil saturation dynamics during waterflood and subsequent injection of liquid CO₂ in the near neutral-wet core sample G23, respectively. Minor fingering effects in the 2D images and an evenly distributed decrease in oil saturation is observed in Figure 5 during waterflooding. The high S_{or, D_2O} of 53.2 % PV is due to the early termination of the waterflood. Figure 6 shows swelling of the oil phase, piston-like displacement and loss of MRI signal during injection of CO₂, leaving a residual oil saturation of 20.3 % PV.

In the last images of the CO₂ injection sequences, the signal disappears behind the CO₂ front, but material balance indicates residual oil saturation of 26.4 % PV, 4.8 % PV and 20.3 % PV for the core plugs P1, P2 and G23, respectively. The absence of MRI signal is likely due to changes in the relaxation properties in the oil phase when mixing with CO₂. Preliminary experiments indicate that there is a non-linear MRI response of signal intensity to oil saturation as the CO₂ content increases that may reflect changes in oil T_1 values. The MRI signal during waterflood, however, is unaffected by the CO₂ effect on the oil signal and should provide a qualitative comparison with the mass balance estimates of saturations. The uncertainty at this time in the MRI properties of the oil-CO₂ mixtures does not allow for reproducible predictions of saturation during the CO₂ flooding process as evident in the variations that appear amongst the different core samples in this study. Additional measurements on oil-CO₂ MRI properties are needed before quantitative information from the images during CO₂ flood can be extracted.

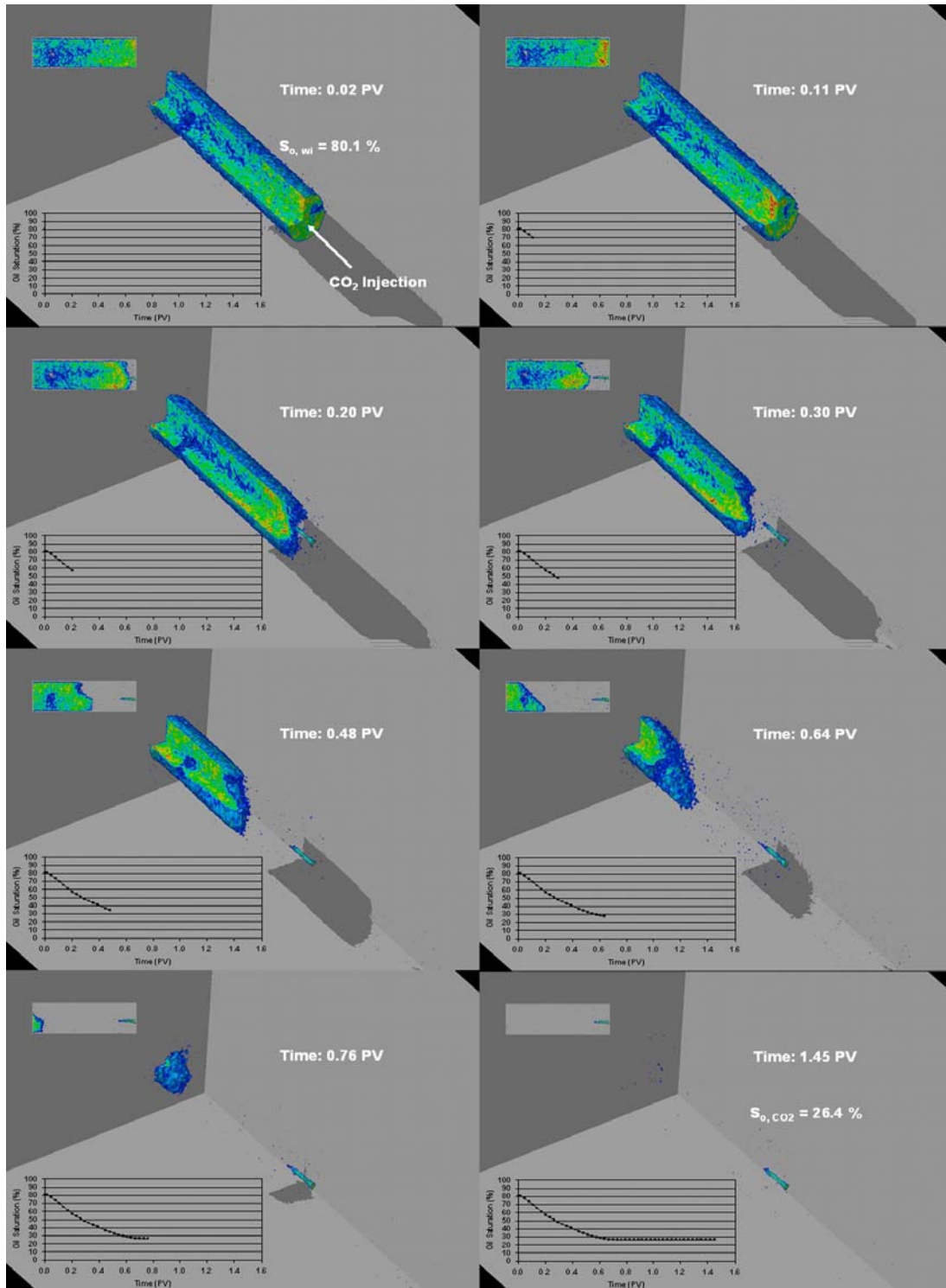


Figure 2. Supercritical CO₂ injection at S_{w_i} in the less water-wet core sample P1.

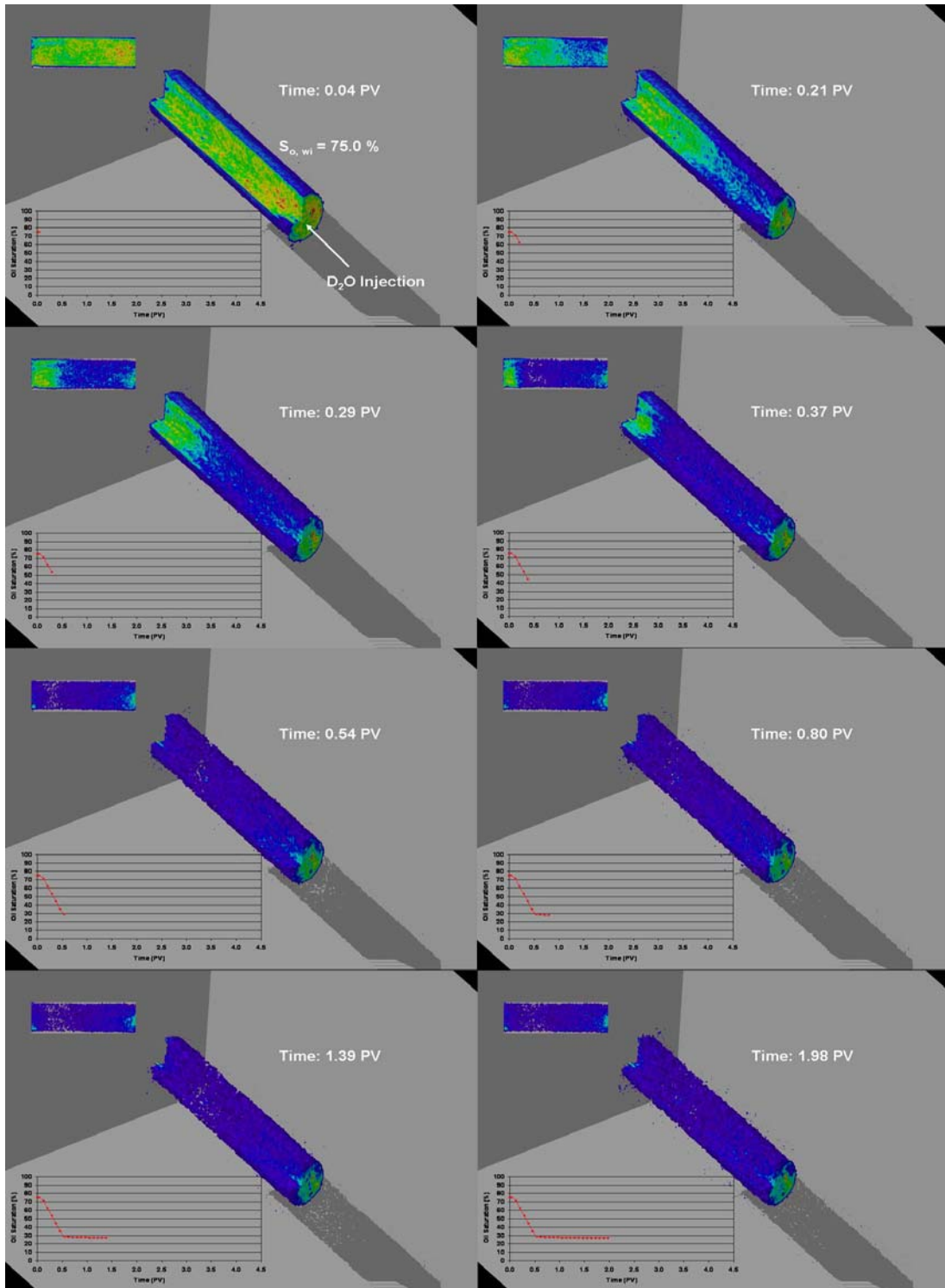


Figure 3. Waterflood of the less water-wet core sample P2.

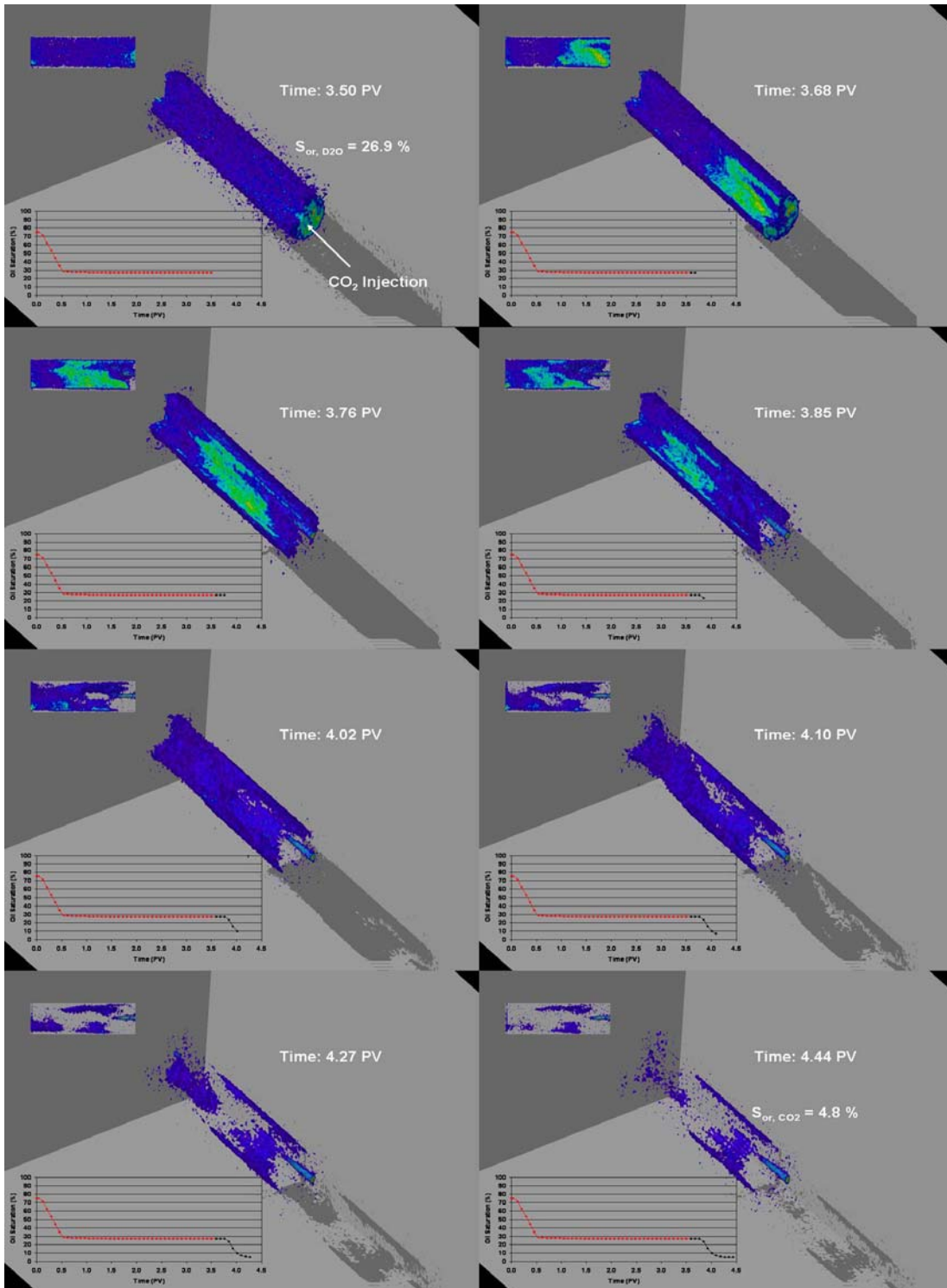


Figure 4. Supercritical CO₂ injection at $S_{or, D2O}$ in the less water-wet core sample P2.

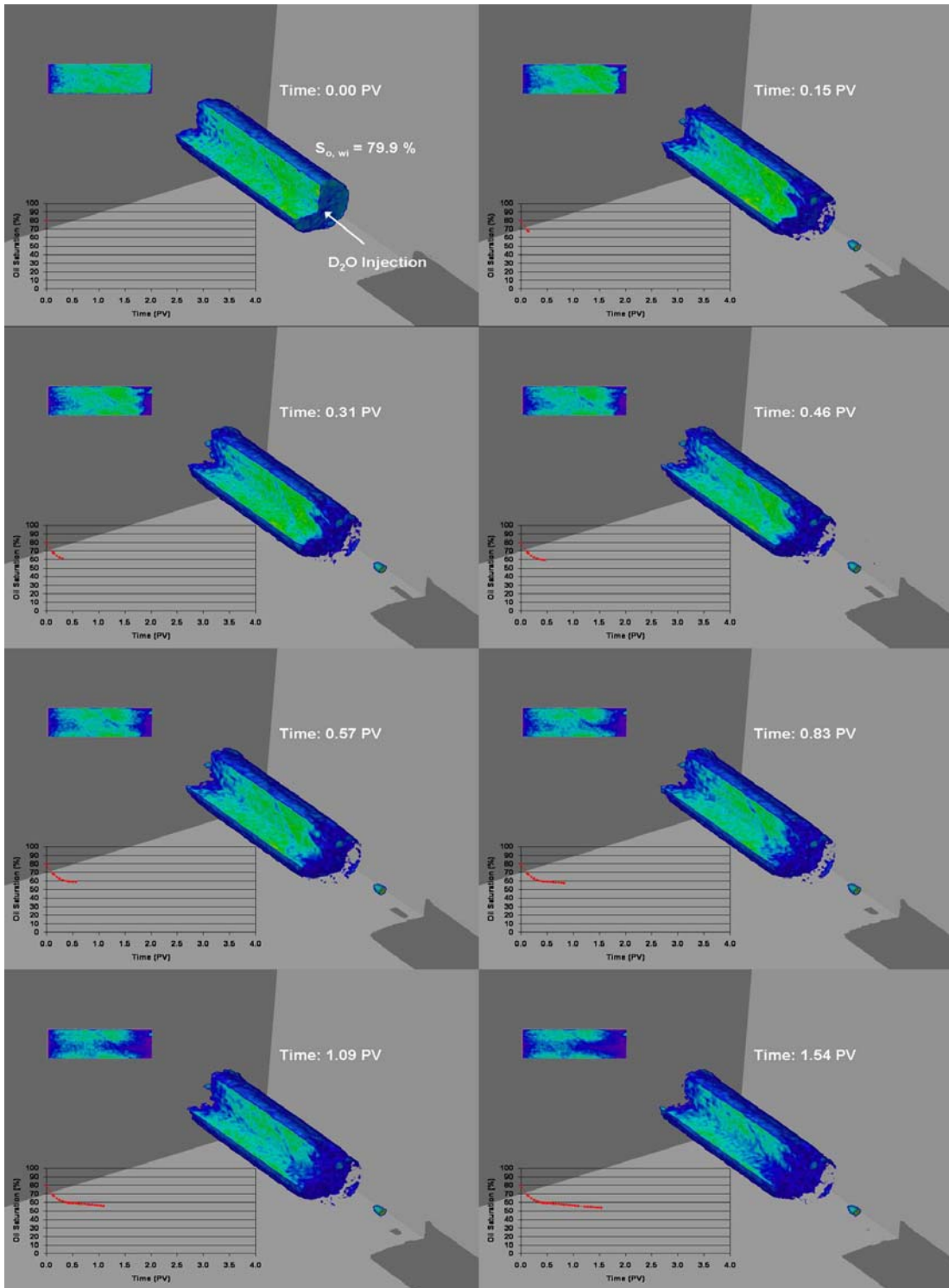


Figure 5. Waterflood of the near neutral-wet core sample G23.

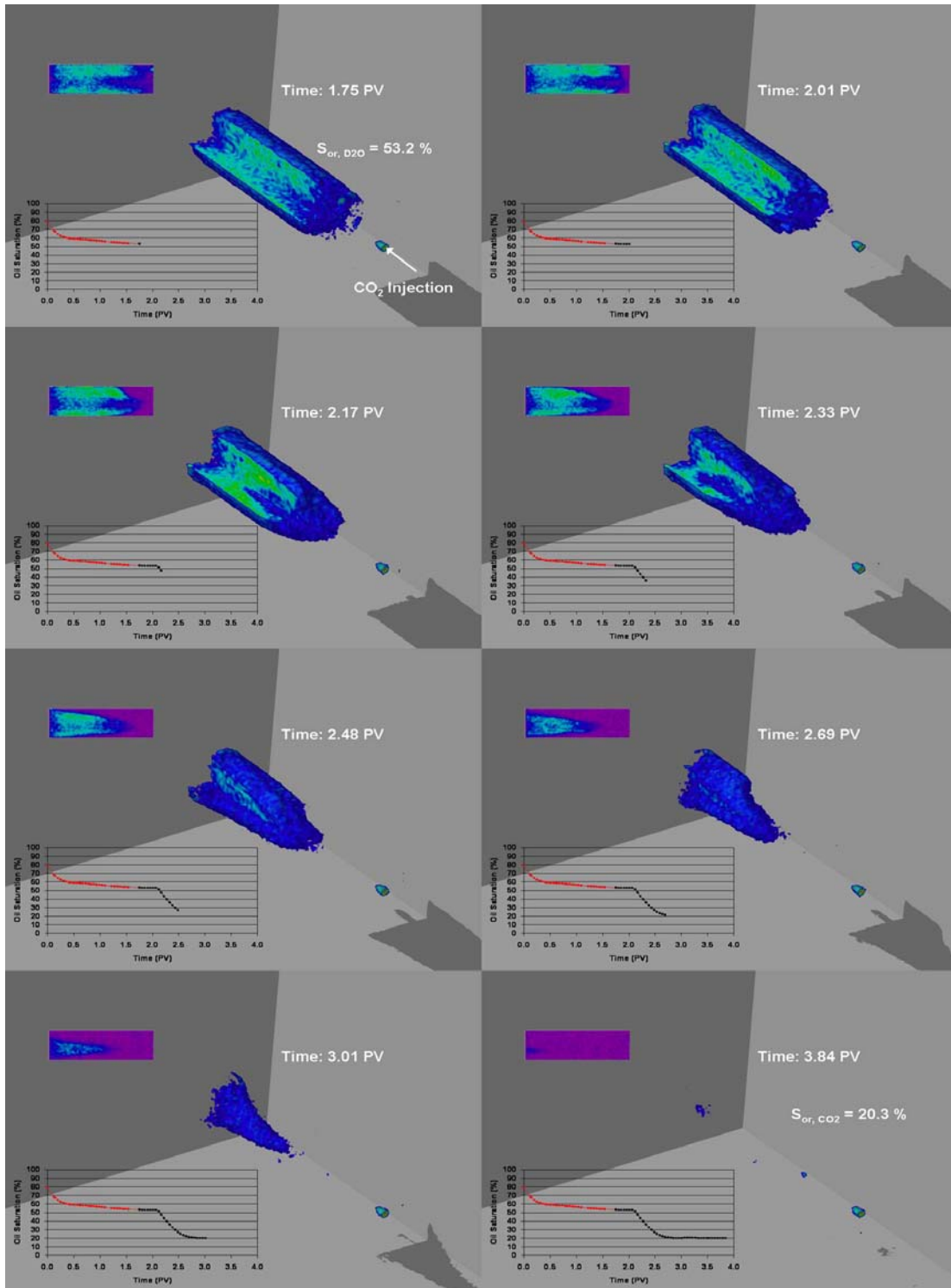


Figure 6. Liquid CO₂ injection at $S_{or, D2O}$ in the near neutral-wet core sample G23.

CONCLUSIONS

- Magnetic Resonance Imaging was used to investigate fluid saturation distributions and to monitor the fluid flow characteristics *in situ* during waterfloods and subsequent injection of either liquid or supercritical CO₂ in four Portland Chalk core samples at different wettabilities.
- Injection of CO₂ at S_{wi} has a lower total recovery factor compared to a waterflood followed by injection of CO₂ at S_{or, D2O}.
- Injection of CO₂ at supercritical conditions exhibits higher total oil recovery than similar injection of liquid CO₂.

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NOMENCLATURE

MMP	:	Minimum Miscible Pressure
MRI	:	Magnetic Resonance Imaging
OOIP	:	Original Oil in Place
R _{f, CO2}	:	Recovery Factor from CO ₂ Injection
R _{f, D2O}	:	Recovery Factor from D ₂ O Injection
R _{f, total}	:	Total Recovery Factor
S _{o, wi}	:	Oil Saturation at Irreducible Water Saturation
S _{or, CO2}	:	Residual Oil Saturation after CO ₂ Injection
S _{or, D2O}	:	Residual Oil Saturation after D ₂ O Injection
S _{w, or, CO2}	:	D ₂ O Saturation at Residual Oil Saturation after CO ₂ Injection
S _{w, or, D2O}	:	D ₂ O Saturation at Residual Oil Saturation after D ₂ O Injection

SI METRIC CONVERSION FACTORS

$$\text{cP} = 10^{-3} \text{ Pa} \cdot \text{s}$$

$$\text{mD} = 0.9869 \cdot 10^{-12} \text{ m}^2$$

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